

Reinhold Environmental Ltd.



2009 NOx-Combustion Round
Table & Expo Presentation

February 9 & 10, 2009, Cleveland, OH

SO₂-SO₃ Oxidation & Thin Wall Thickness

NO_x Roundtable, Cleveland OH
February 10, 2009

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We are shaping the future

ALSTOM

Agenda

- **SO₃ Formation and Impact on Performance**
 - Formation of SO₃
 - Impact on Performance
 - Factors Impacting SO₃ formation
- **Thin Wall Oxidation Reduction**
 - Test procedure
 - Adsorption of SO₃
 - Influence of NH₃
 - Surface Area (Area Velocity)
 - Temperature
- **Catalyst Manufacturing Types**
- **Thin Wall Stability**
- **Conclusion**

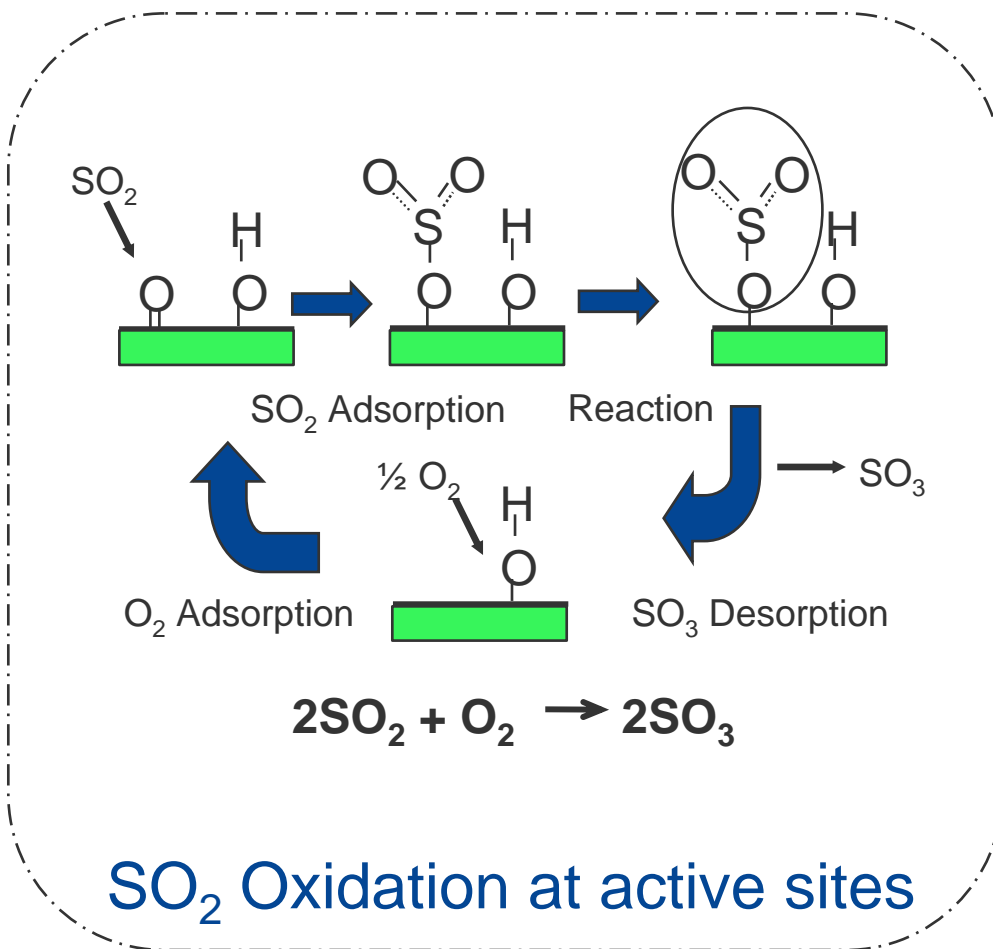
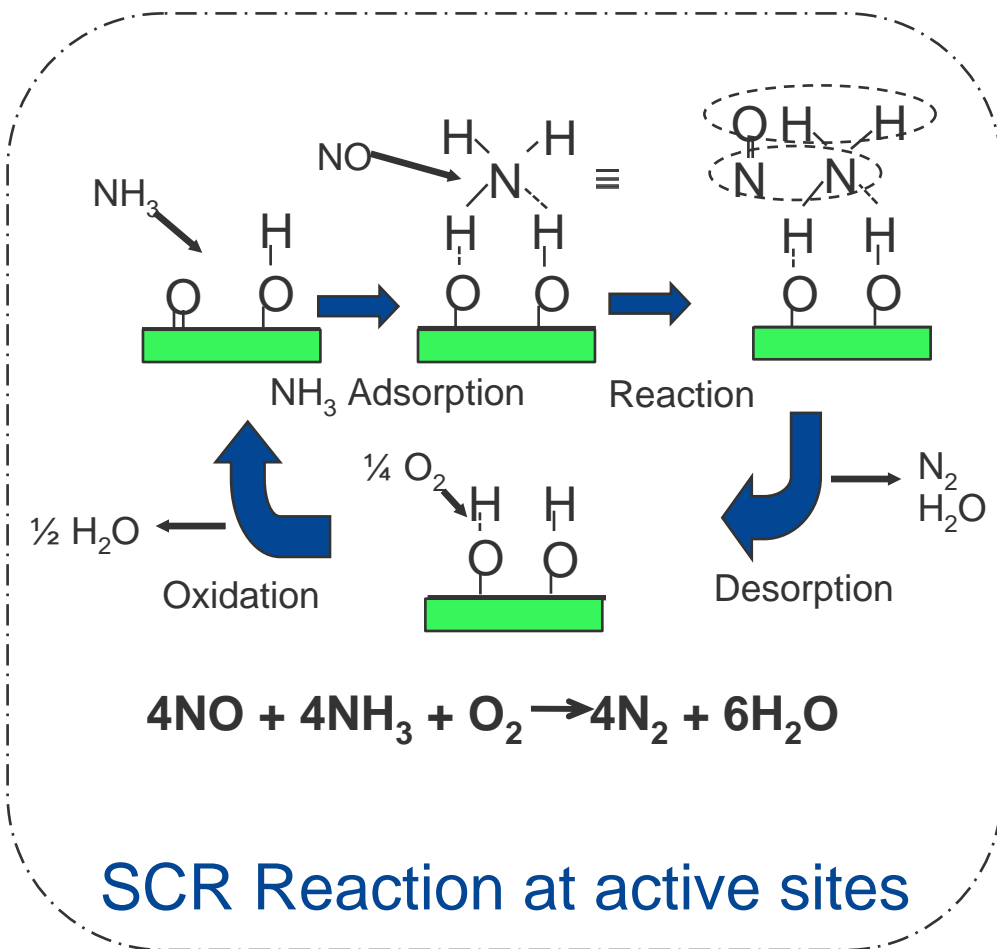
SO₃ Formation and Impact on Performance

- SO₃ Formation and Impact on Performance
 - Formation of SO₃
 - Impact on Performance
 - Factors Impacting SO₃ formation

SO₃ Formation

- During combustion, sulfur existing in fuel, is converted into SO₂
- At the Inlet of SCR reactor, SO₃ is contained approx. 1% of total SO_x
- SO₂ is adsorbed with Vanadium, the main reagent in active SCR catalysts, and is oxidized into SO₃
- SO₂ oxidation rates are determined by the activity of the SCR catalyst

Reactions at Catalyst's Active Sites

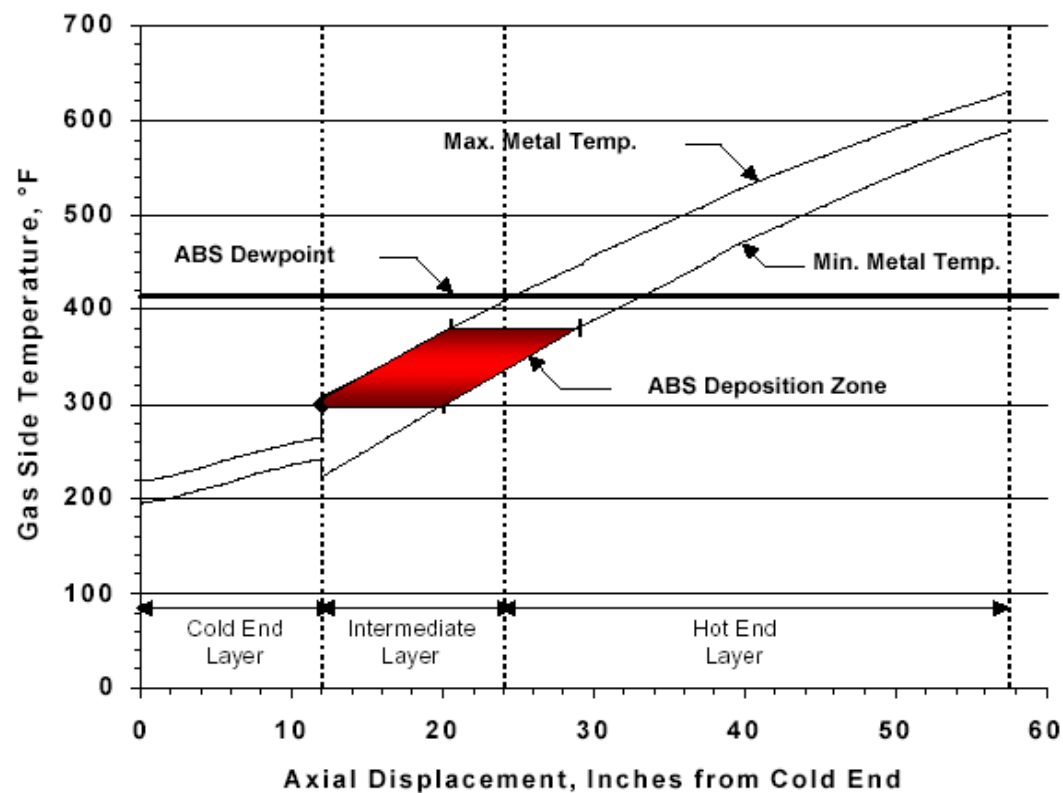
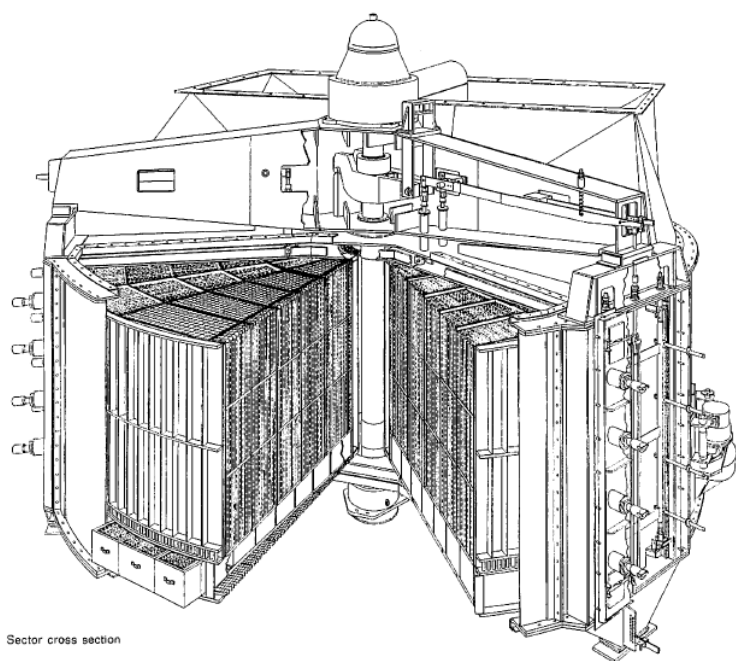


SO₃ Formation Impact

- Both Ammonium Sulfate, (NH₄)₂SO₄, and/or Ammonium Bisulfate, NH₄HSO₄, are formed within a critical temperature zone when flue gas contains various levels of SO₃
- Critical temperature zone typically occurs at the Air Pre-Heater
- The sulfur content found in most American coals results in Ammonium Bisulfate, NH₄HSO₄ formation
- Ammonium Bisulfate, NH₄HSO₄, causes Air Pre-Heater plugging

NH₄HSO₄ Impact on the Air Pre-heater

- “Sticky” Ammonium Bisulfate, NH₄HSO₄, causes Air Pre-Heater plugging



NH₄HSO₄ Impact on the Air Pre-heater

- “Sticky” Ammonium Bisulfate, NH₄HSO₄, causes Air Pre-Heater plugging

Cold End Layer (upper face)

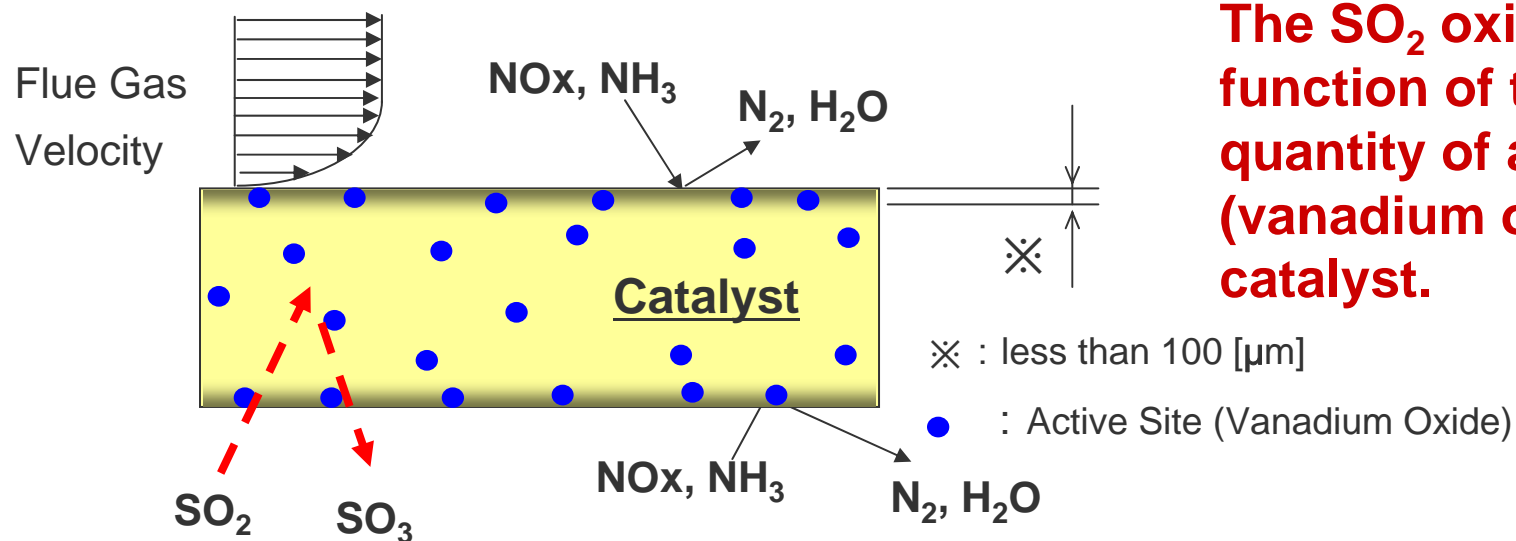


Intermediate Layer (side view)

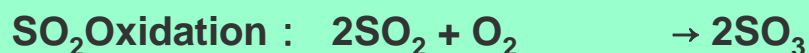
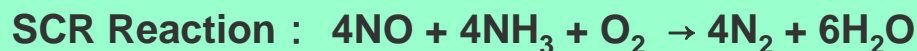


SO₃ Formation – Catalyst Mass

- The SCR reaction is a fast reaction that occurs within the 100 microns of a catalyst surface.
- Unlike the SCR reaction, SO₂ oxidation occurs **throughout** the catalyst mass.



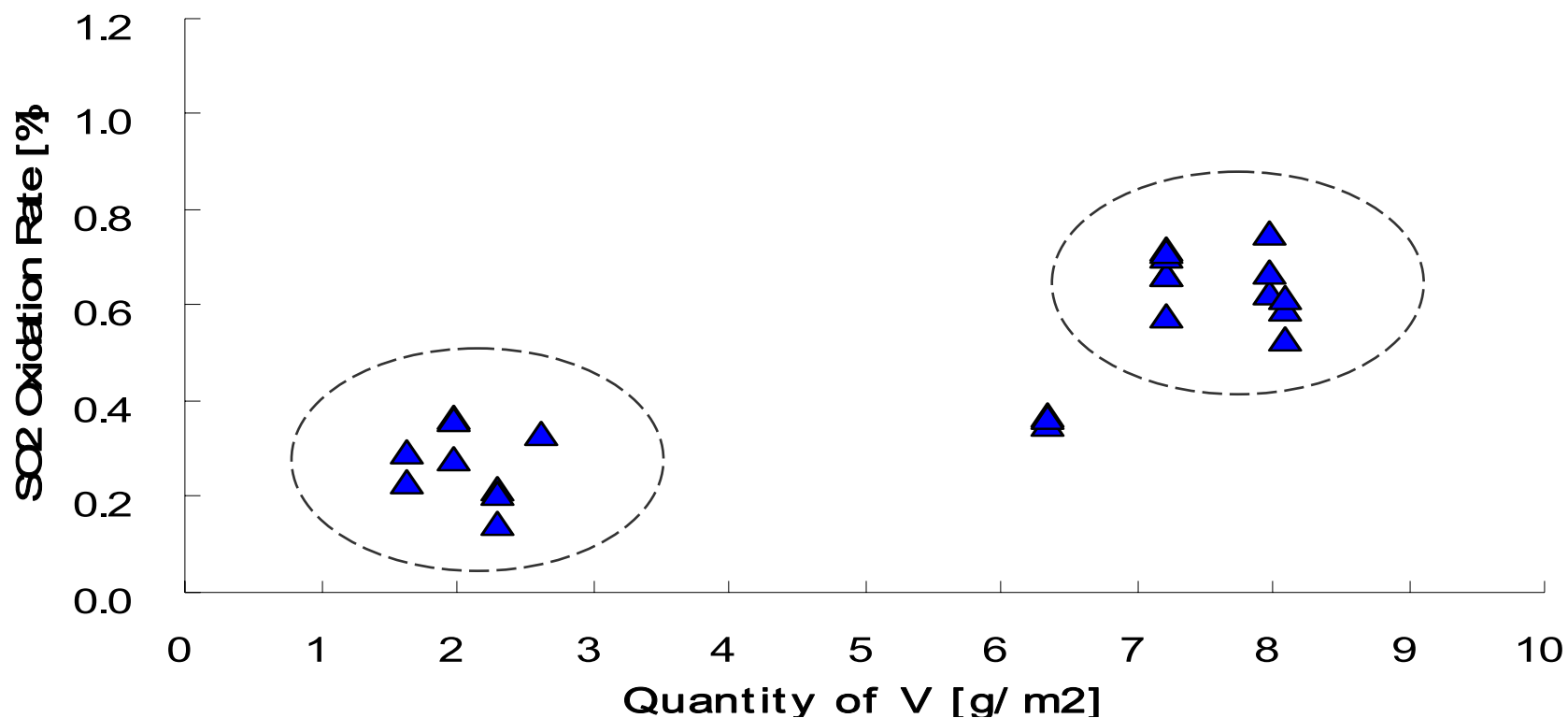
The SO₂ oxidation rate is a function of the total quantity of active sites (vanadium oxide) in the catalyst.



Reducing SO₂ Oxidation – Vanadium Content

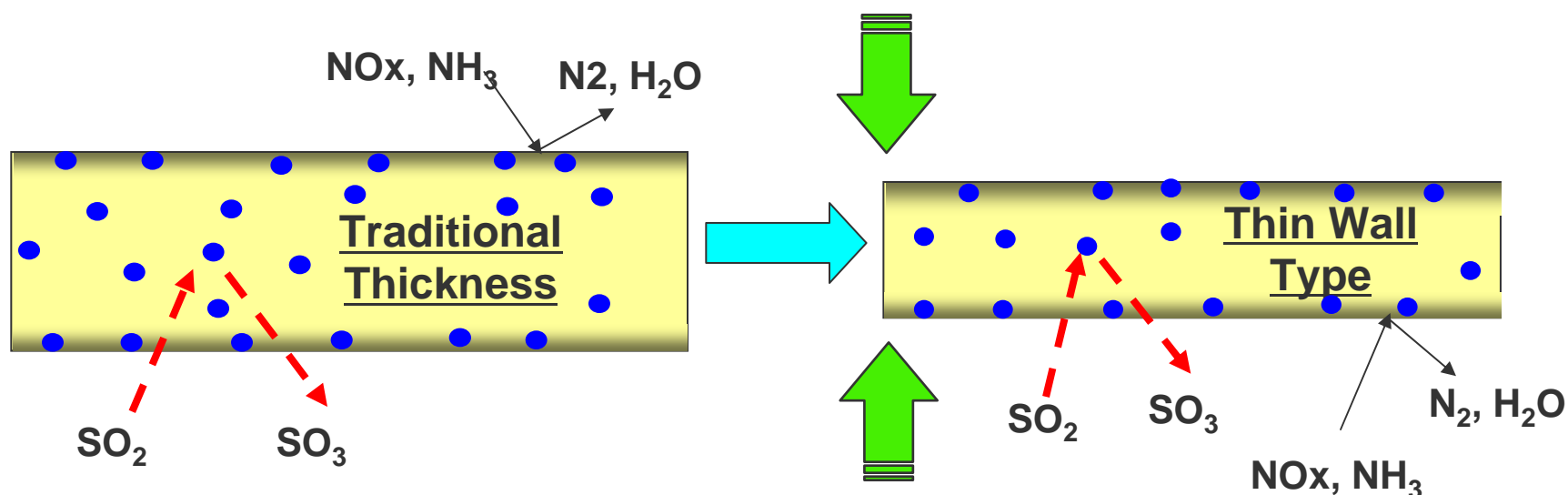
SO₂ Oxidation Rate

Temp.: 400°C(752degF), AV = 10Nm/ h
(Inlet SO₂: 2800ppm)



Reducing SO₂ Oxidation

- Although the thickness has been reduced, the “density” of the active site at the catalyst’s surface has not changed.
- There is no differences in the NOx Reduction Rate after reducing the Catalyst thickness.
- **There IS a reduction in SOx Oxidation Rate!**



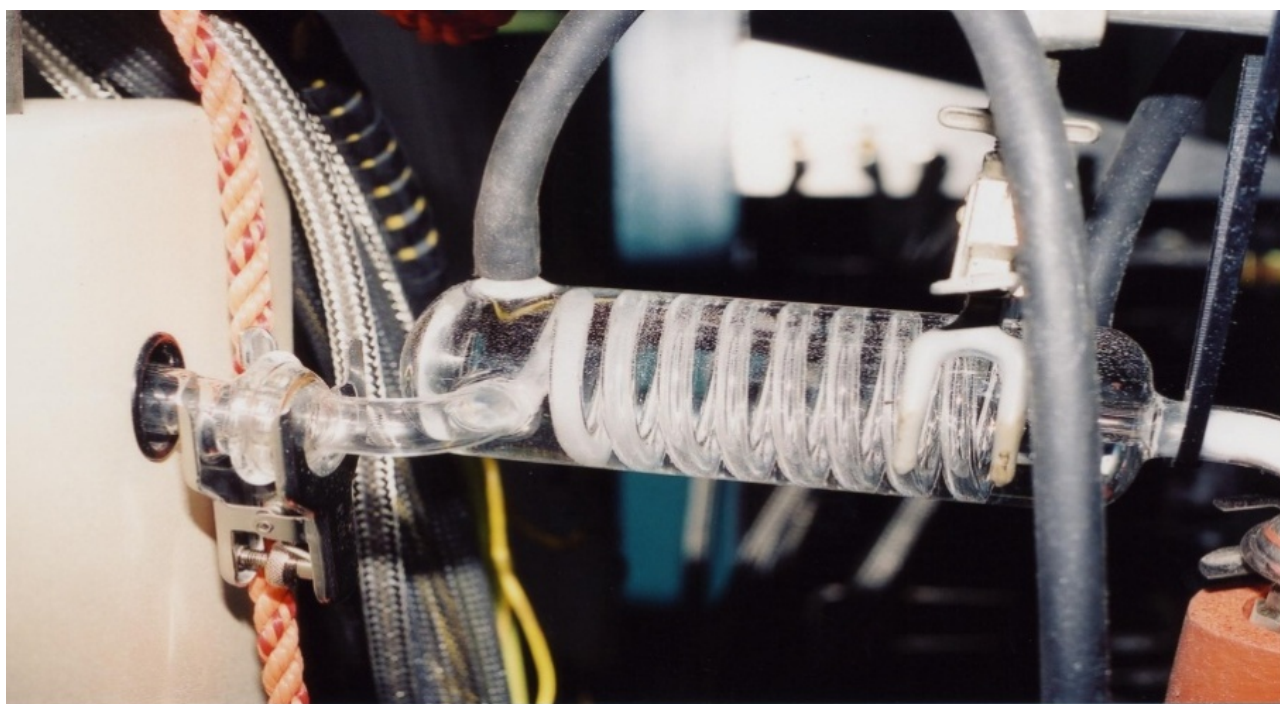
Thin Wall Oxidation Reduction

• Thin Wall Oxidation Reduction

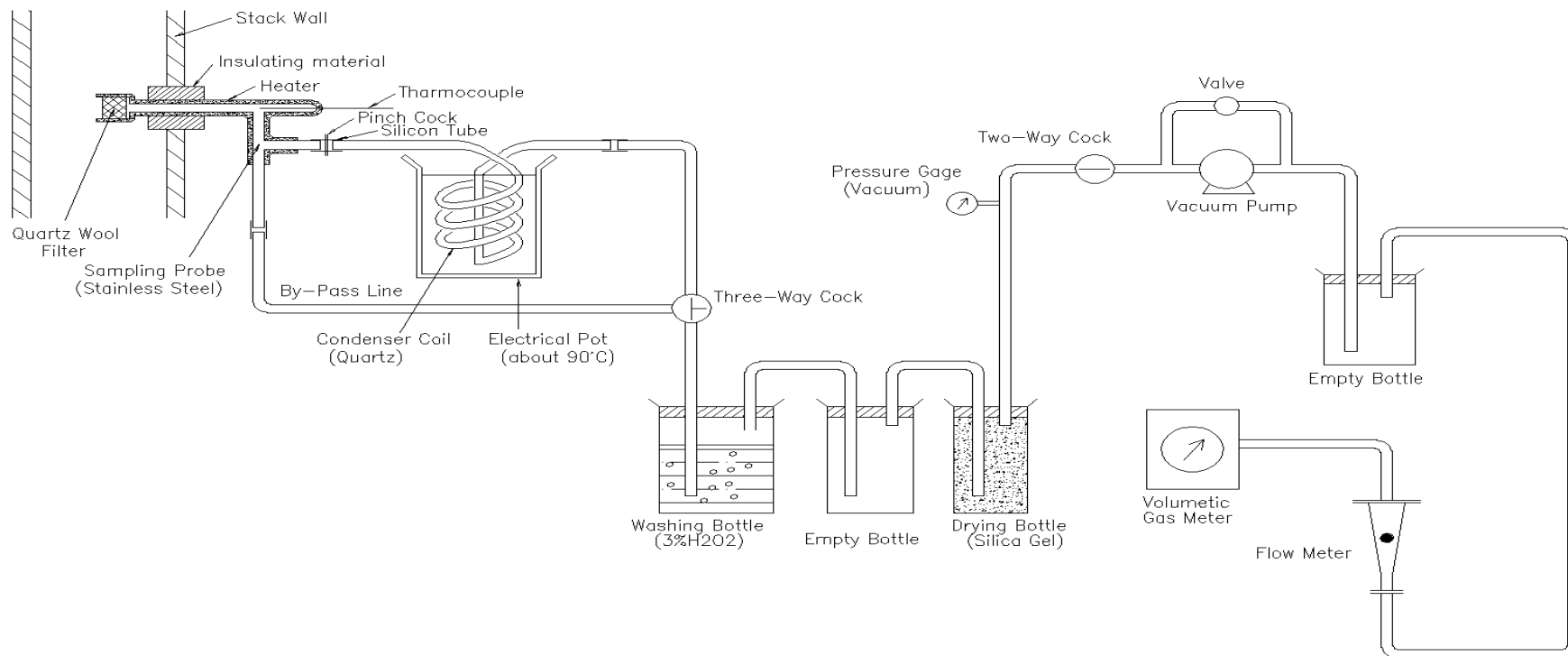
- Test procedure
- Adsorption of SO_3
- Influence of NH_3
- Surface Area (Area Velocity)
- Temperature

Measuring SO₃ for Determining SO₂ Oxidation Rate

- To measure SO₃, we utilized the “Helical Tube Capture Test”
- The Helical Tube is very effective for accurate measurement of SO₃



SO₃ Sampling Train for Testing



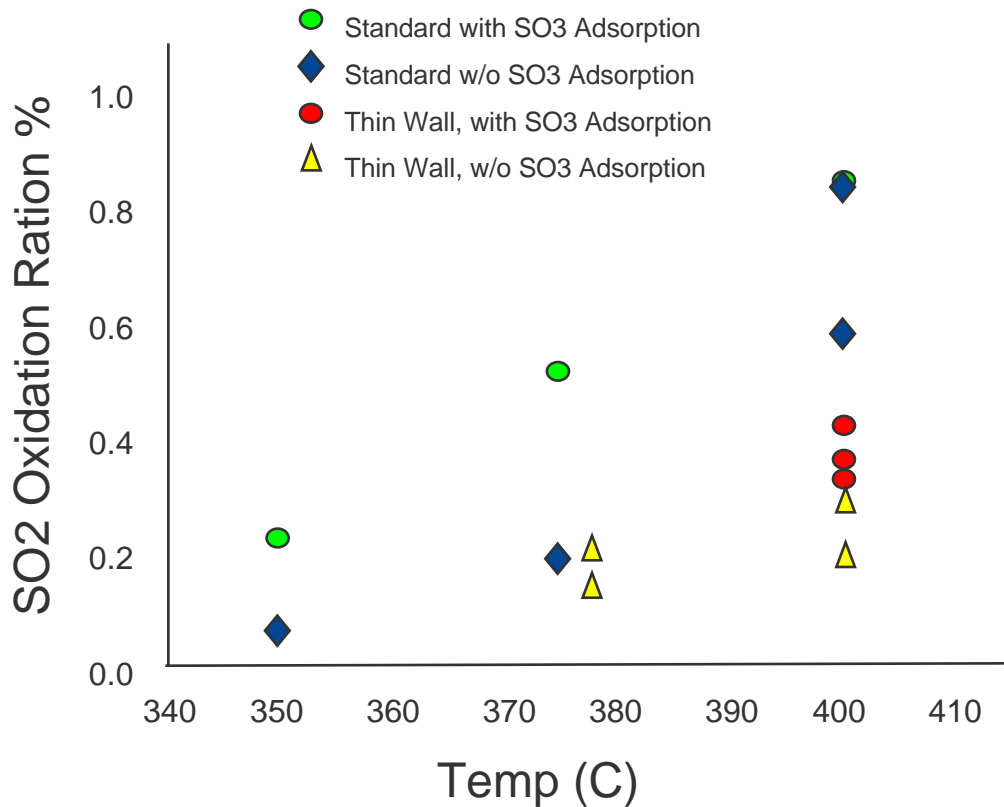
Schematic Diagram of Sampling Train for SO₃ measuring

Test Procedure

- A bench scale apparatus with 4 catalyst layers was used.
- The control catalyst was the K-Max substrate.
- The following parameters were controlled to simulate the actual gaseous operating conditions of the SCR reactor;
 - Gas composition,
 - Temperature,
 - Gas velocity and catalyst's area velocity,
 - NH₃ volume ratio.

SO₃ Adsorption & SO₂ Oxidation Rate

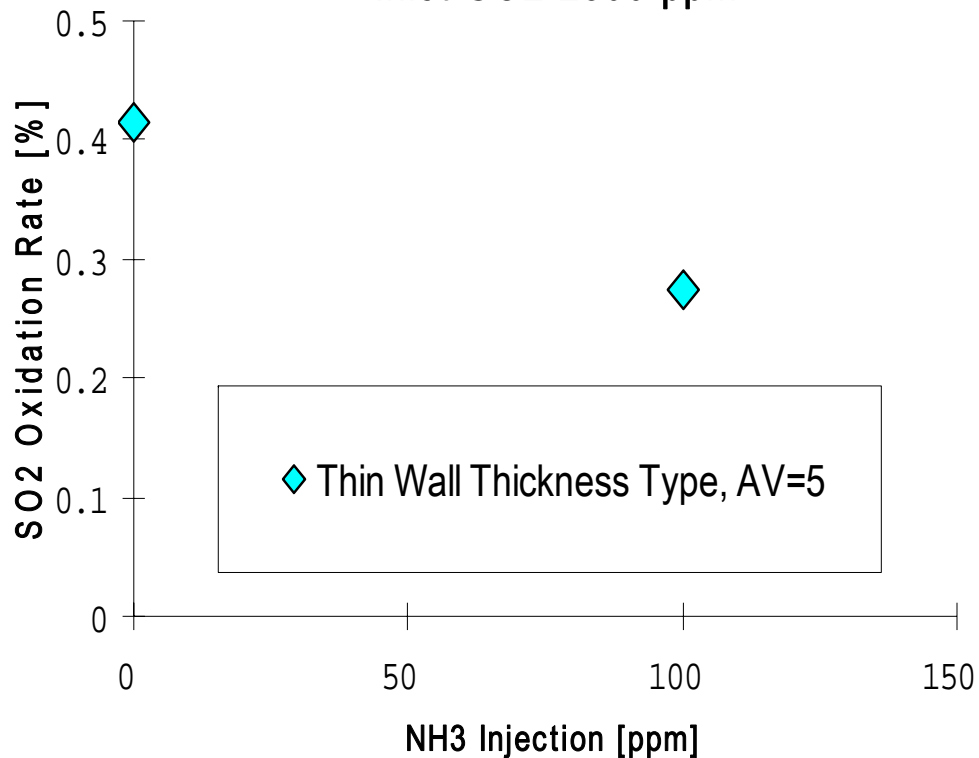
Impact of SO₃ Adsorption



- At startup, SO₃ is adsorbed onto the catalyst layer for up to 50 hours
- Up to 50 hours there is a natural increase until saturation
- This phenomenon is temperature dependent
- At 400C There is a higher trend for SO₂ oxidation
- Thin Wall thickness maintains lowest rate of Oxidation

NH₃ Influence for SO₂ Oxidation

Impact of NH₃ Injection
at 400degC, W/O NO_x
Inlet SO₂ 2800 ppm



- 0.4mm-thick.
- No NO_x in this test
- Entire catalyst surface is exposed by same concentration of NH₃ [ppm].
- Captured active sites by NH₃ limits the SO₂ oxidation.
- IMPACT: Lower rates of NH₃ results in Higher Rates of SO₂ oxidation

Definition of Area Velocity

Definition of Area Velocity:

$$AV = Q / A$$

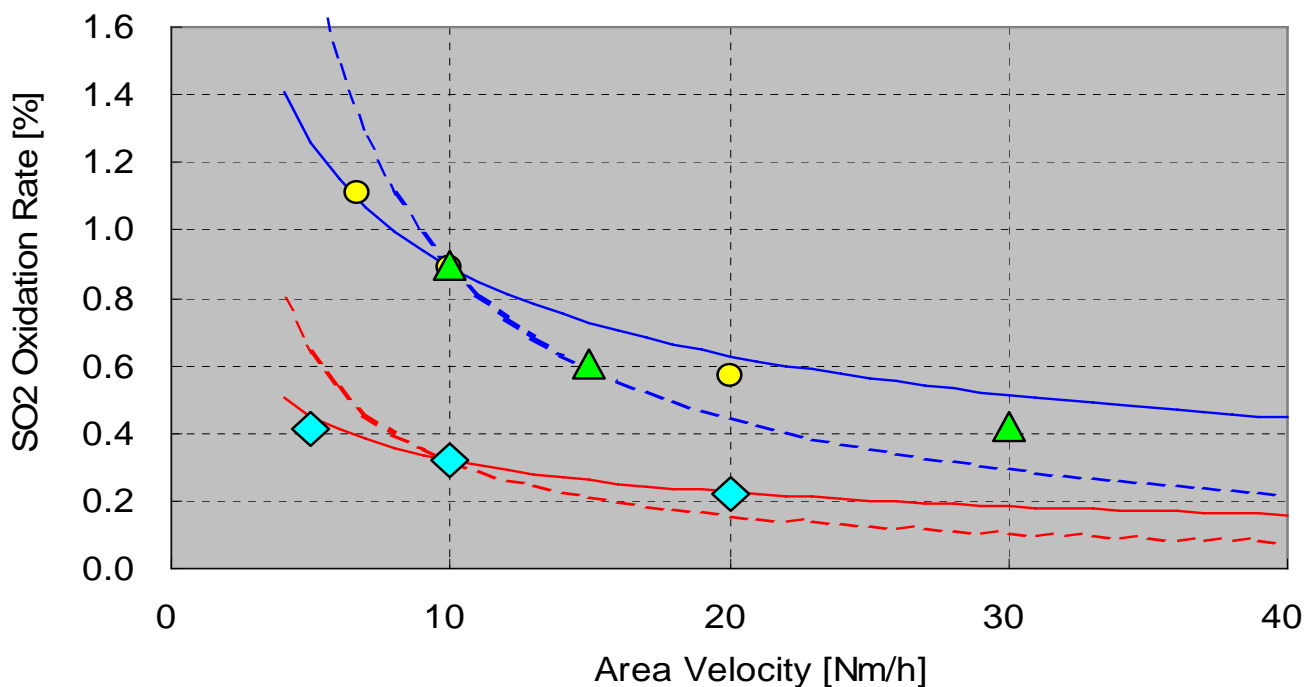
AV= Area Velocity [$\text{Nm}^3/\text{m}^2 \cdot \text{hr}$]

Q = Flue gas flow rate [Nm^3/hr]

A = Contact Surface Area [m^2]

Impact of Area Velocity @400degC(752degF)

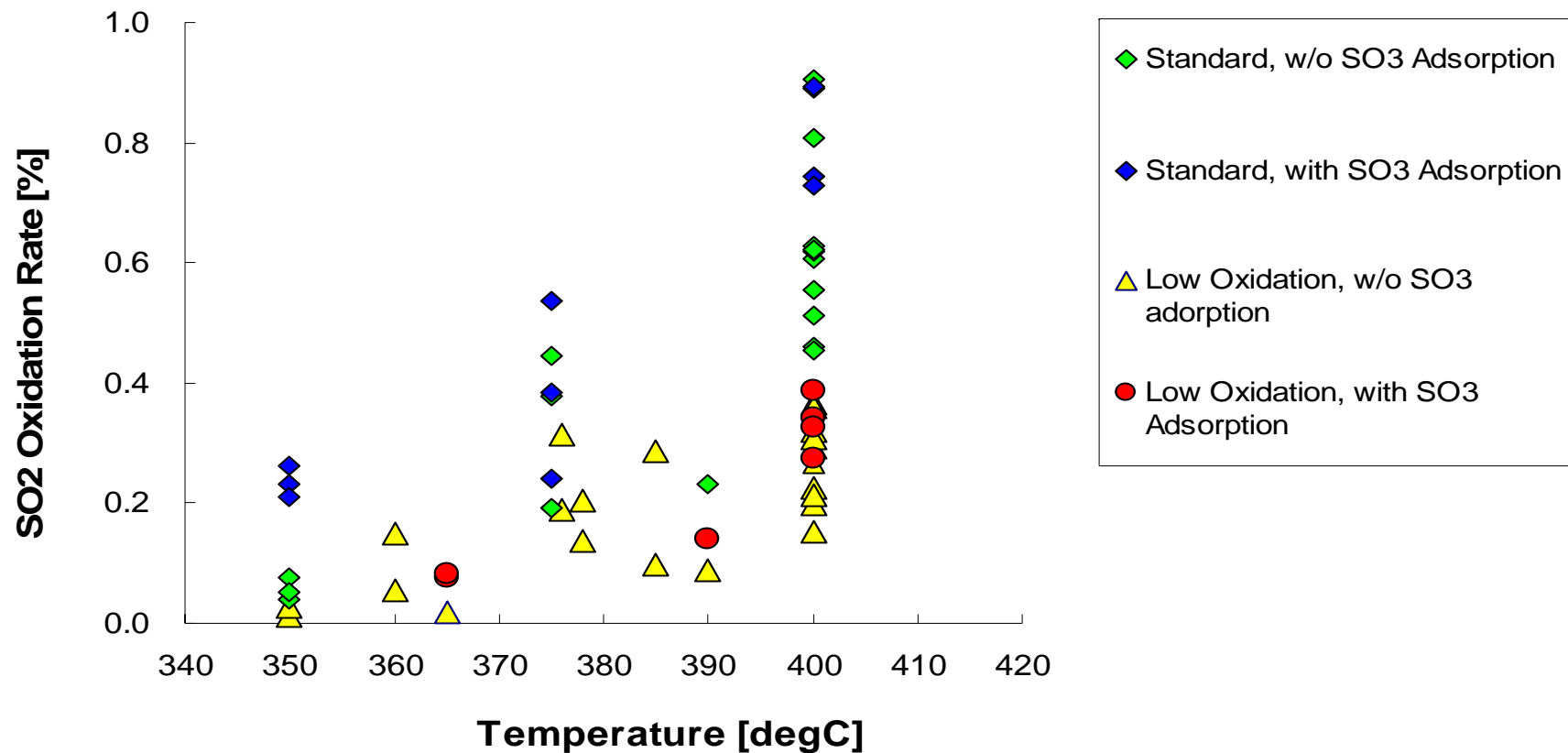
Impact of Area Velocity (at 400°C, Without NH3 Injection)



- ◆ Low Oxidation Type, (with SO3 Adsorption)
- Standard Type (Before SO3 Adsorption)
- ▲ Standard Type (with SO3 Adsorption)
- (AV/10)^{0.5} for Low Oxidation Type
- - - (AV/10) for Low Oxidation Type
- (AV/10)^{0.5} for High Oxidation Type
- - - (AV/10) for High Oxidation Type

Impact of Temperature for SO₂ Oxidation Rate

SO₂ Oxidation Rate
(AV = 10 Equivalent, Inlet SO₂: 2800ppm)



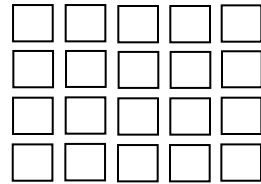
Testing Summation

- 1) SO₂ oxidation rate depends on the catalyst's Vanadium Content
- 2) Adsorption rate increases after the initial ~50hrs of operation
- 3) NH₃ impacts oxidation rates, More NH₃=Less Oxidation
- 4) As temperature increases, SO₂ Oxidation increases
- 5) As Area Velocity increases SO₂ Oxidation decreases
- 6) Thin Wall catalysts maintained the lowest rates of oxidations for all the aforementioned variables

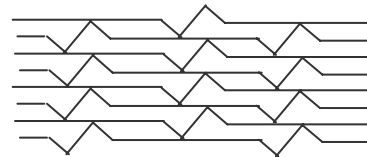
Catalyst Manufacturing Types

- Catalyst Manufacturing Types

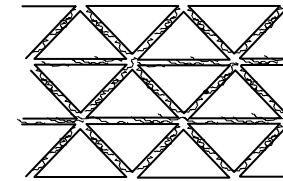
Catalyst Manufacturing History and Variation



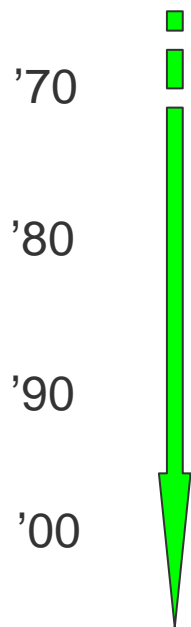
Extrude
Honeycomb



Plate



Triangular
Corrugated



Extrude Type



Plate Type



Triangular /Metal Plate

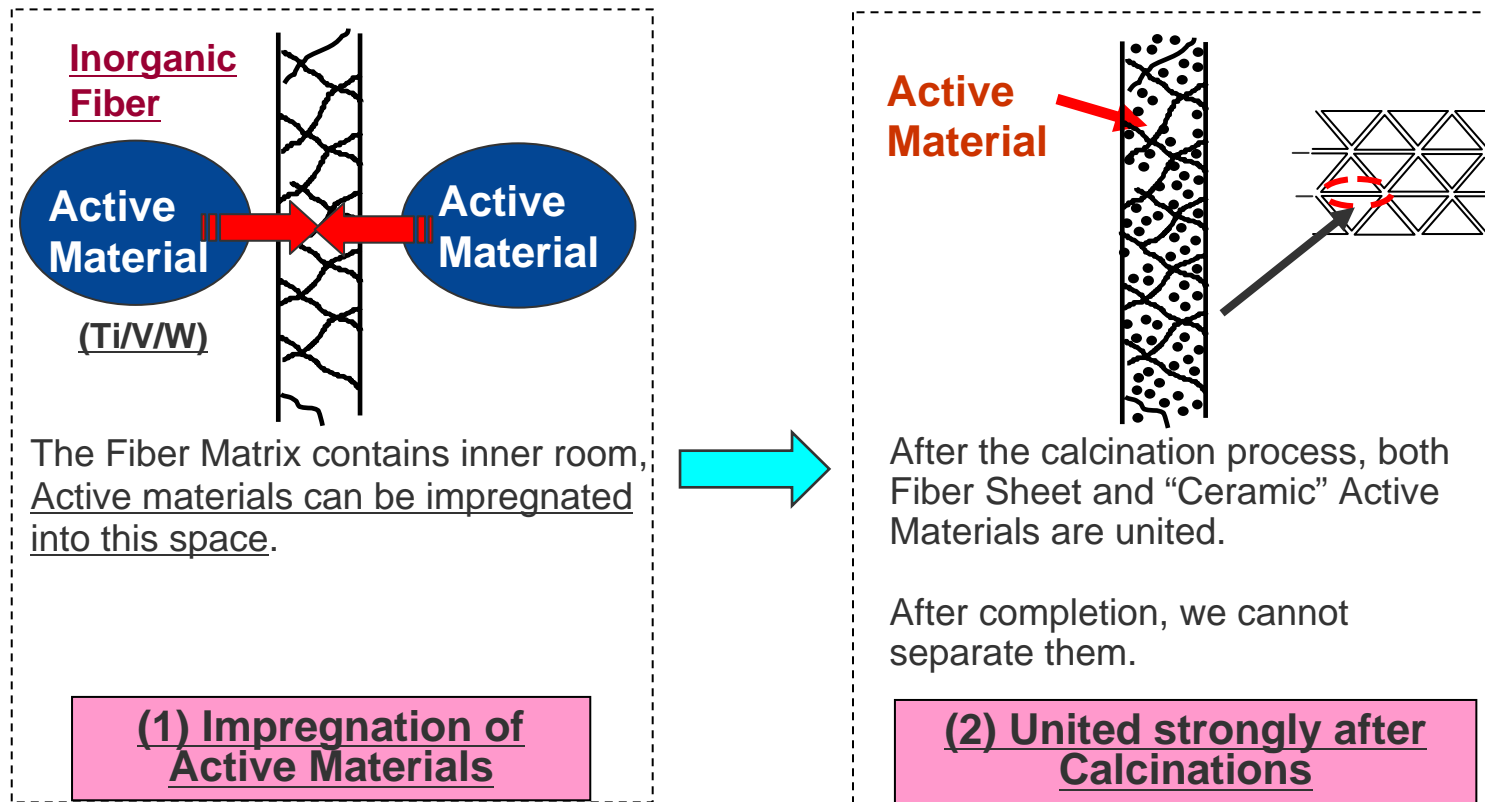


Triangular /Hybrid



Corrugated Catalyst Manufacturing

- (1) Catalyst Active Material are impregnated inside of the Fiber Matrix.
- (2) Both Active Materials and Fibers are united after calcification.



Thin Wall Stability

- Thin Wall Stability

P 25

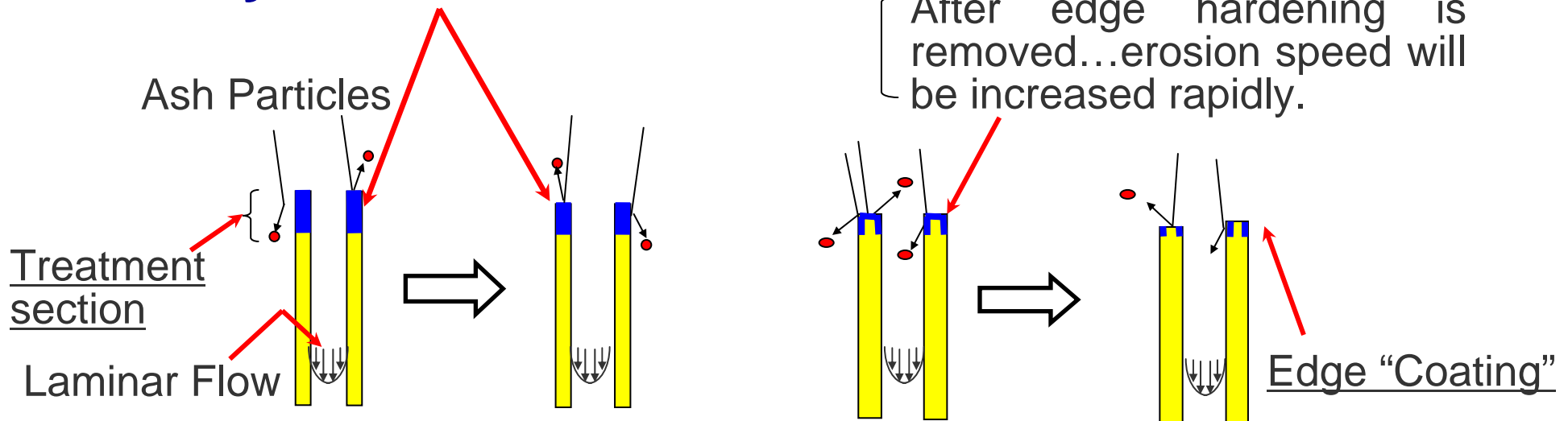
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Deep vs. Edge Hardening

Always Same Hardness



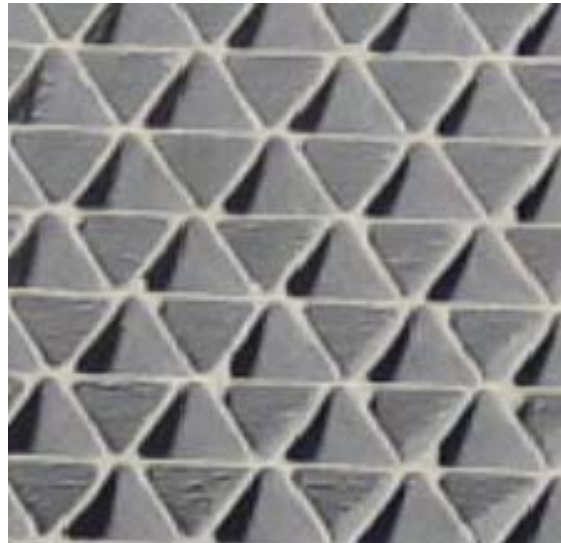
Deep Treatment for K-MAX Catalyst

Edge Coating

- Since this "Hardening Treatment" is applied not only the surface but also the inside of catalyst monolith, the erosion speed is the same.

Deep Hardened Application

Deep Hardening for Catalyst



- (1) Catalyst End Facing Incoming Gas**
(after several years operation in Taiwan Plant)

Deep vs. Edge Hardening

Deep Hardened Catalyst

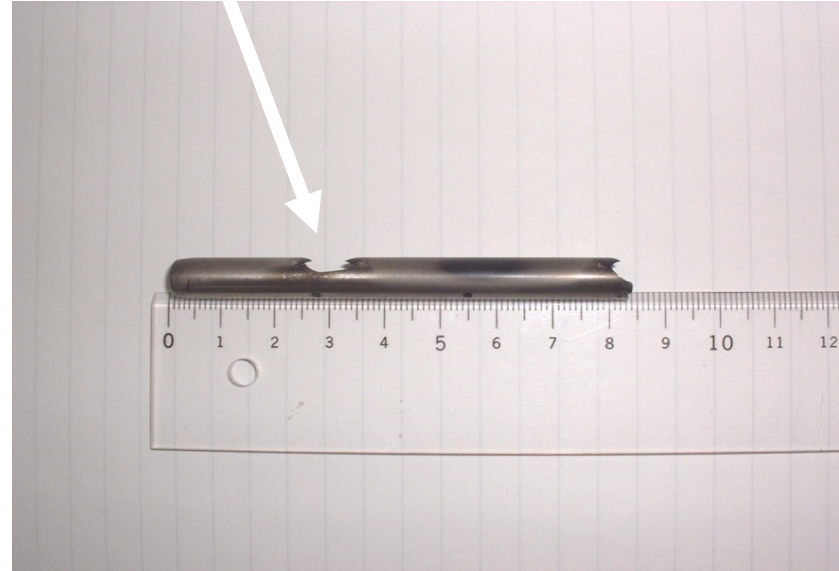


Edge Hardened Catalyst



Thin Wall Toughness

Damaged Stainless Steel Tube



- At Ontario Power, during a performance test the Stainless Steel tube, located above the catalysts, was broken by flyash erosion. There was NO damage to the catalyst.

Thin Wall Catalyst

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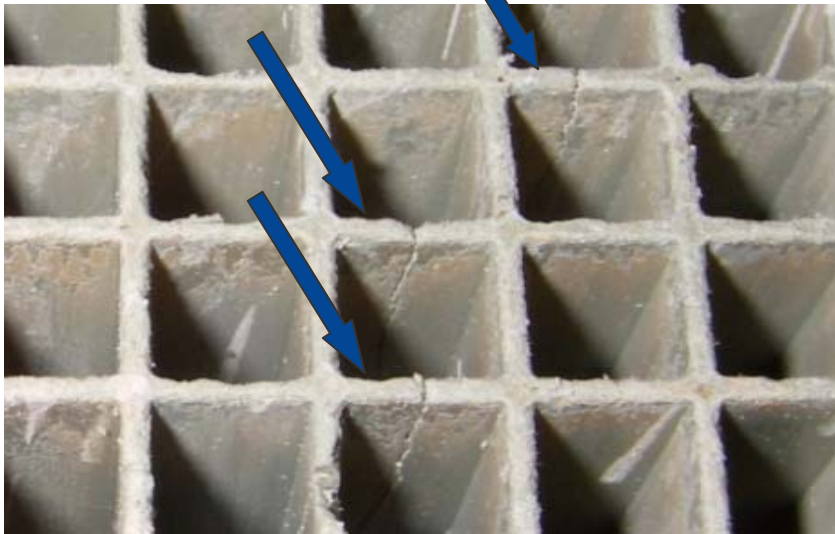
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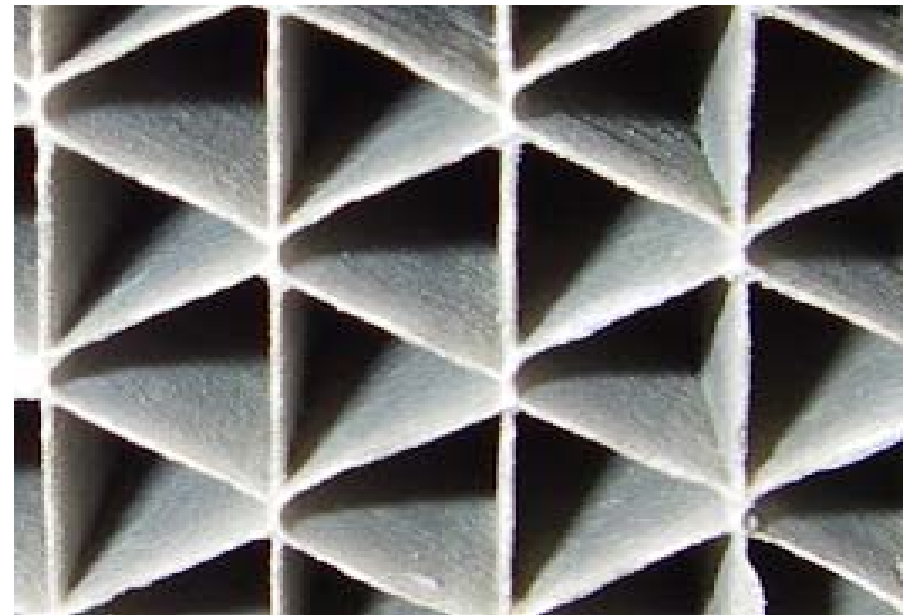
Fiber Matrix Tough

- Inside a SCR system the temperature change can be up to 100 deg F
- Typical Catalysts can receive “Thermal Shock”
- Thin Wall fiber matrix resists “Thermal Shock”

Thermal Cracks



Operated
Extruded Type Cat.

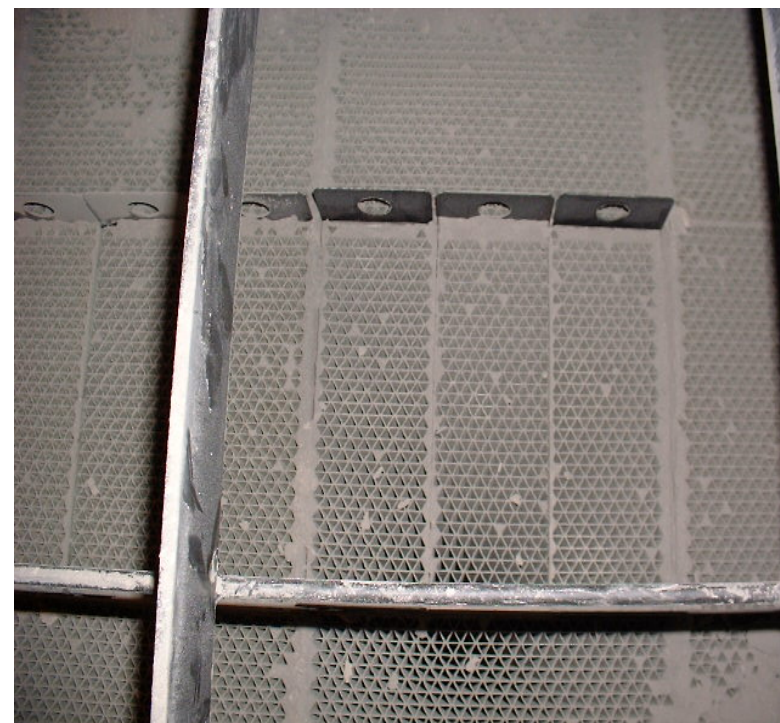
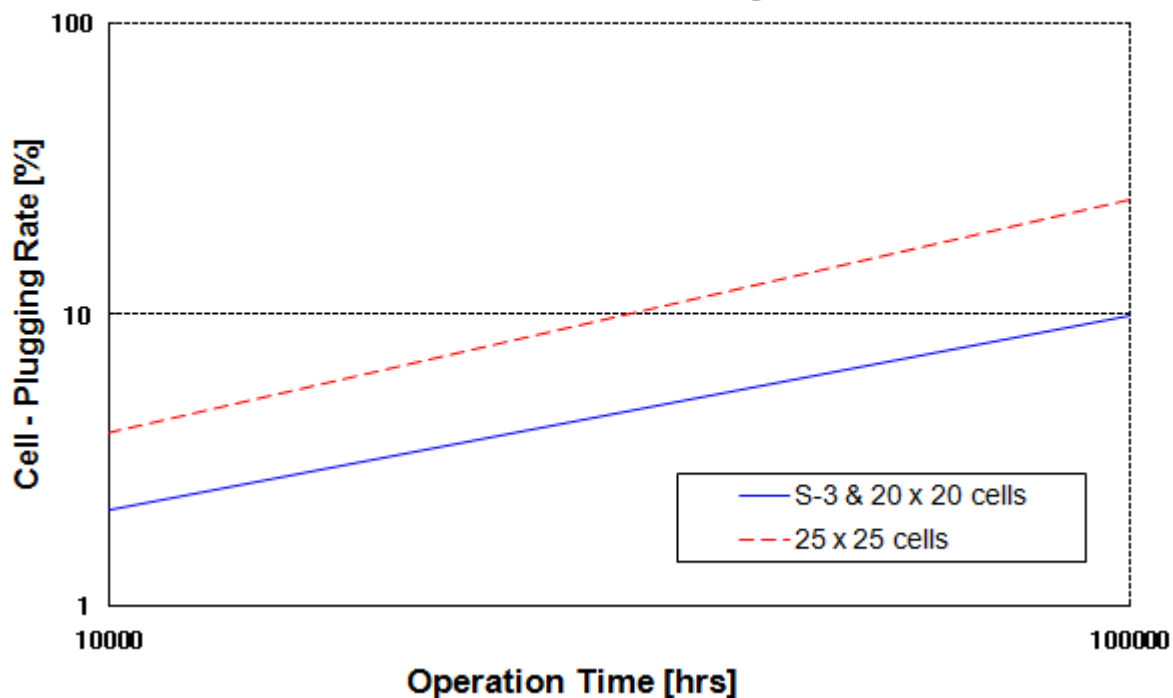


Operated
Thin Wall

High Density, Thin Wall, Low Plugging

Thin Wall catalyst provides high geometric surface area, it's plugging rate is less than the 25x25 cell honeycomb catalyst, which has similar density.

Cell - Plugging Rate (Bit. Coal, $LV \approx 2 \text{ Nm/s}$)
< Center Area of Each Catalyst Modules >

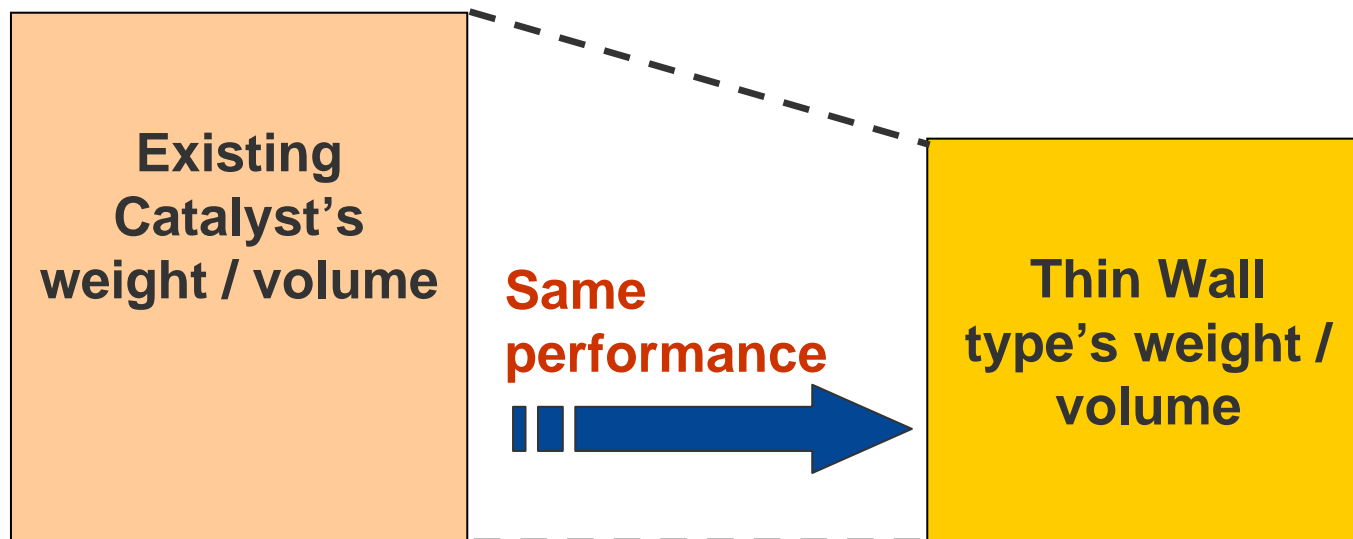


Additional Thin Wall Advantages

HIGH SUBSTRATE DENSITY

“Thin Walls = Less Total Volume” and “Light Weight”

We can achieve the same Area Velocity (= same SCR Performance) w/o any modifications of Reactor



Additional Thin Wall Notes

- **Thin Wall Catalysts can be Regenerated**
 - **Regeneration of Thin Wall Catalyst requires special consideration**
 - **Regeneration techniques may vary from traditional regeneration techniques**
 - **Requires careful washing**
 - **Apply Chemical treatment to remove poisoning**
 - **Re-apply a Chemical treatment of active materials**
- **Thin Wall Catalyst washing is not recommended by users without guidance**
 - **This is due to the wide variation in customer washing techniques**
 - **To ensure proper protection of the Active materials when considering washing, consult your catalyst manufacturer**

Conclusion

- Ammonium Bisulfate at Pre-heater is one of the biggest issue regarding the SCR Catalyst due to SO₃ formation
- Wall Thickness influences the SO₂ oxidation
- Thin Wall Thickness maintains the NO_x reaction, while minimizing the SO₂ oxidation
- Thin Walls using Fiber Matrix manufacturing technology are as, if not more durable than traditional catalyst manufacturing methods
- Fiber Matrix corrugated catalysts have less plugging, and higher density than traditional catalysts, while minimizing SO₂ oxidation

Questions? Comments?

**Please visit the ALSTOM booth for
any further discussions, and to
view actual catalyst materials.**

Thank you!

